

# Universal dependence of hydrogen oxidation and evolution reaction activity of platinum-group metals on pH and hydrogen binding energy

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Understanding how pH affects the activity of hydrogen oxidation reaction (HOR) and hydrogen evolution reaction (HER) is key to developing active, stable, and affordable HOR/HER catalysts for hydroxide exchange membrane fuel cells and electrolyzers. A common linear correlation between hydrogen binding energy (HBE) and pH is observed for four supported platinum-group metal catalysts (Pt/C, Ir/C, Pd/C, and Rh/C) over a broad pH range (0 to 13), suggesting that the pH dependence of HBE is metal-independent. A universal correlation between exchange current density and HBE is also observed on the four metals, indicating that they may share the same elementary steps and rate-determining steps and that the HBE is the dominant descriptor for HOR/HER activities. The onset potential of CO stripping on the four metals decreases with pH, indicating a stronger OH adsorption, which provides evidence against the promoting effect of adsorbed OH on HOR/HER.

## INTRODUCTION

The alkaline environment of hydroxide exchange membrane fuel cells and electrolyzers (HEMFCs and HEMELs, respectively) opens up the possibility of using nonprecious metals as catalysts; HEMFCs and HEMELs, in turn, become an affordable alternative to the precious metal-reliant proton exchange membrane fuel cells and electrolyzers (PEMFCs and PEMELs, respectively) (1–8). Only a negligible fraction of precious metal, as well as cost, is on the negative electrode in PEMFCs and PEMELs, owing to the extremely fast hydrogen oxidation reaction (HOR)/hydrogen evolution reaction (HER) kinetics in the acidic environment. However, the sluggish kinetics of HOR/HER in alkaline media—two orders of magnitude slower than that in acid on Pt (9–11), Ir (11), and Pd (11)—necessitates higher precious metal loadings on the negative electrode at equivalent overpotential and could offset, to a large extent, the lowered cost from the use of nonprecious metal-based catalysts on the positive electrode.

Despite recent discussion in the literature on the potential role of adsorbed OH for HOR in base (12, 13), hydrogen binding energy (HBE) has been shown to be the dominant descriptor for HER/HOR activity (11, 14–16). Volcano-shaped curves have been obtained when plotting HER activity versus HBE on various monometallic metals in base (14) as well as in acid (17–19), suggesting that an optimal HBE exists (Sabatier's principle). Recent studies on the HOR/HER activity of Pt at different pH values suggest that the pH of electrolytes affects HOR activity by modifying the HBE of catalysts. For example, slower HOR/HER kinetics in base coincides with higher HBE calculated from cyclic voltammograms (CVs) (15). More recently, Wang *et al.* (16) have shown that PtRu alloy is twice as active as Pt for HOR in alkaline media in spite of the lower onset potential for adsorbed OH on the latter, indicating that the oxophilicity of catalysts does not play a major role in facilitating HOR. Despite growing evidence on specific systems, the general correlation between HOR activity and HBE and between HBE and pH among different metals remains to be elucidated. Establishing

such correlations on precious metals, which are stable over a broad pH range and hence ideal model systems, will set the stage for the rational search for nonprecious metal-based HOR catalysts.

Here, we demonstrate the generality of the effect of pH (0 to 13) on HBE and, in turn, of HBE on HOR/HER activities, in terms of exchange current densities ( $i_0$ ), on supported platinum-group metal (Pt, Ir, Pd, and Rh) nanoparticles (Ru was not studied because it is susceptible to oxidation in the hydrogen adsorption/desorption potential region). We show that the HBE of each metal increases linearly with pH with a similar slope, indicating that the effect of pH on HBE is independent of metal. We also show that the  $\log(i_0)$  of each metal decreases linearly with HBE with a similar slope, which indicates a universal correlation of  $i_0$  with HBE and provides strong evidence that HBE is the dominant descriptor for HOR/HER activities. Furthermore, the onset potential for adsorbed OH, as indicated by CO stripping experiments, decreases monotonically with pH, indicating that the facilitating role of adsorbed OH in HOR is minimal.

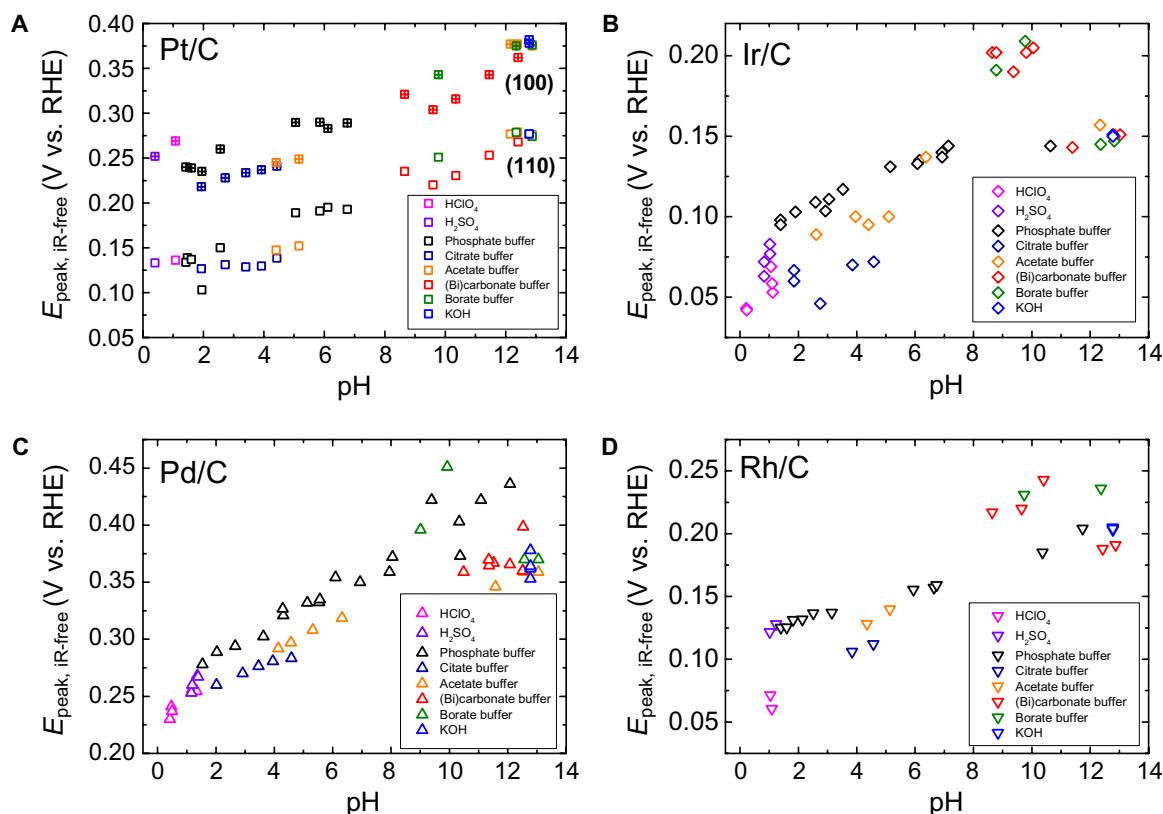
## RESULTS

### pH-dependent HBEs of Pt/C, Ir/C, Pd/C, and Rh/C

Desorption peaks for underpotential deposited hydrogen ( $H_{\text{upd}}$ ) on carbon-supported Pt, Ir, Pd, and Rh nanoparticles (Pt/C, Ir/C, Pd/C, and Rh/C) all shift to more positive potentials as the pH of the electrolyte increases, indicating that the increase of HBE with pH is a general trend (Fig. 1). The desorption peak potentials ( $E_{\text{peak}}$ ) were obtained from the respective CVs recorded in buffered electrolytes with pH ranging from 0 to 13 (fig. S1). Two distinctive  $H_{\text{upd}}$  adsorption/desorption peaks corresponding to Pt(110) (located at a lower overpotential) and Pt(100) (located at a higher overpotential) are clearly visible in CVs of Pt/C (fig. S1A) over the entire pH range tested. Both peaks rise almost linearly with pH (0 to 13) (0.12 to 0.27 and 0.22 to 0.37 V for the 110 and 100 facets, respectively), with a slope of 13 mV/pH for Pt(110) and 12 mV/pH for Pt(100) (Fig. 1A), which corresponds reasonably well with reported values for polycrystalline Pt [10 mV/pH for Pt(110) and 8 mV/pH for Pt(100) (15) or ~11 mV/pH for both facets (20)] and

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**Fig. 1. Underpotential deposited hydrogen ( $H_{\text{upd}}$ ) desorption peak potential as a function of pH.** (A to D)  $H_{\text{upd}}$  desorption peak potentials from CVs of (A) Pt/C, (B) Ir/C, (C) Pd/C, and (D) Rh/C as a function of pH.

high-index single-crystalline Pt [10 mV/pH for Pt(553) and Pt(533)] (21). Similar correlations between  $E_{\text{peak}}$  and pH were observed on Ir/C, Pd/C, and Rh/C (Fig. 1, B to D), with slopes of 9, 11, and 10 mV/pH for Ir/C, Pd/C, and Rh/C, respectively. The similar linear correlation and slope observed for all four metals suggest the generality of the effect of pH on  $E_{\text{peak}}$ . The positive shift of  $E_{\text{peak}}$  represents an increase in HBE from acid to base. Given the prominent role that HBE plays in determining the HOR/HER activities on monometallic Pt-group metal catalysts (15), it is likely that pH affects the HOR/HER activity mainly through the tuning of HBE, as shown for Pt/C, Ir/C, Pd/C, and Rh/C in the following section.

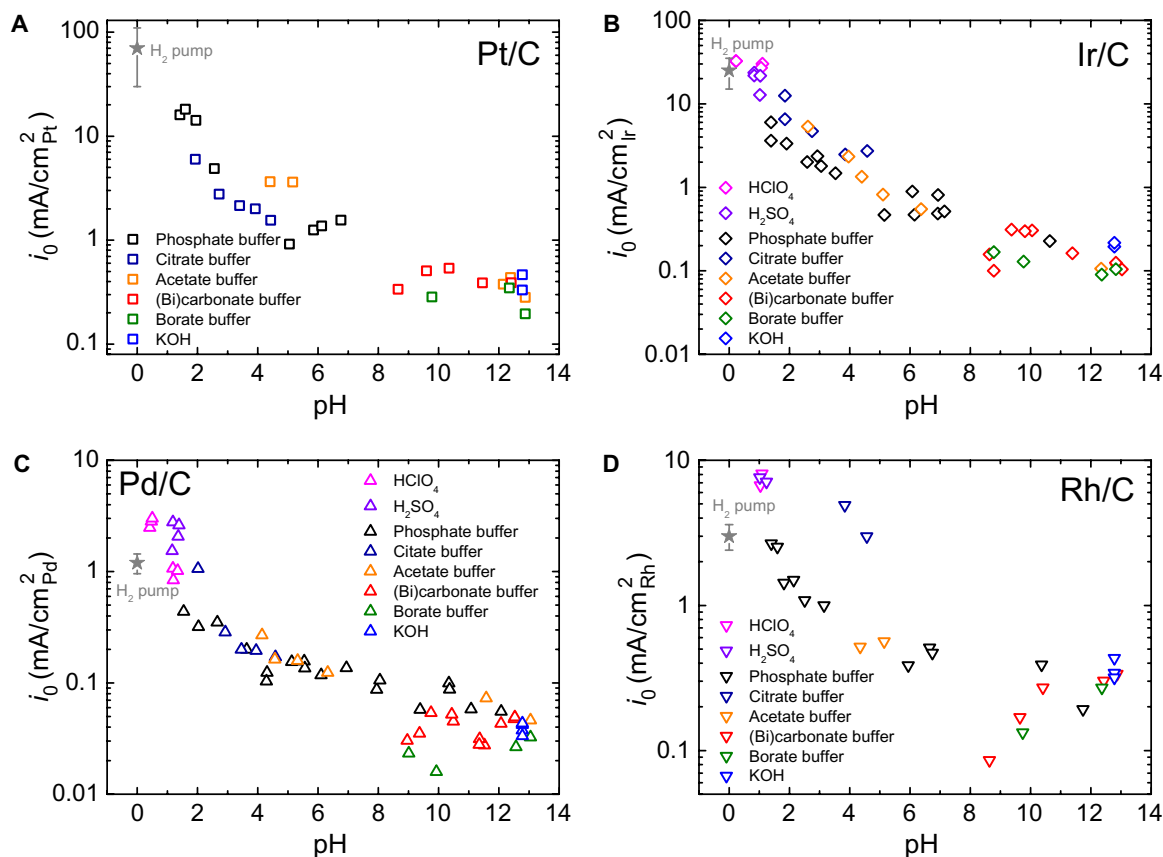
#### pH-dependent HOR/HER activities on Pt/C, Ir/C, Pd/C, and Rh/C

The HOR/HER activities on Pt/C, Ir/C, Pd/C, and Rh/C, determined using the rotating disk electrode (RDE) method, decrease monotonically with rising pH (Fig. 2), consistent with the theory that higher HBE suppresses catalytic performance. We used buffer solutions to avoid the deviation of pH at the electrode surface from the bulk (22) so that reliable kinetic data could be obtained (15). We used multiple buffer solutions, that is, phosphoric acid/phosphate, citric acid/citrate, acetic acid/acetate, carbonate/bicarbonate, and boric acid/borate, and their effectiveness in eliminating local concentration was confirmed by the lack of a plateau in the HER portion of the HOR/HER polarization curves (figs. S2 to S5). Exchange current densities ( $i_0$ ), which represent the intrinsic HOR/HER activities, were obtained by normal-

izing to the electrochemical surface area of the catalysts (figs. S2 to S6) in the same electrolyte used for activity measurements. The  $\log(i_0)$  of all four catalysts decreases monotonically with pH (Fig. 2). Because the HBE of the four metals increases with pH, our results confirm that higher HBE leads to lower HOR/HER activities, thus providing strong evidence supporting HBE as the dominant performance descriptor for HOR/HER catalysts. In addition, only small variations were observed for both  $E_{\text{peak}}$  and HOR/HER activities measured in different buffer solutions with similar pH values (Figs. 1 and 2), indicating that the nature and adsorption of anions do not have any significant effect on the results. This finding is reasonable because anion adsorption typically occurs above the potential of zero charge (PZC),  $\sim 0.57$  V versus reversible hydrogen electrode (RHE) for Pt (23), whereas HOR/HER proceeds below the PZC. Our  $i_0$  values of Pt/C, Ir/C, Pd/C, and Rh/C at 293 K at low pH are in agreement with those measured in an  $H_2$ -pump with a PEMFC configuration, wherein pH is presumed to be zero and reactions are, in principle, free of  $H_2$  transport limitation (gray stars in Fig. 2) (24). This agreement confirms the reliability of our activity measurements, especially for those in the acidic environment.

#### Universal correlation between HOR/HER activity and HBE

A universal linear correlation between  $\log(i_0)$  and  $E_{\text{peak}}$  (that is, HBE) is obtained for Pt/C, Ir/C, Pd/C, and Rh/C (Fig. 3). The  $x$  axis in Fig. 3 ( $E_{\text{peak}}$ ) can be converted to HBE according to the formula  $\text{HBE} = -FE_{\text{peak}} - \frac{1}{2}TS_{\text{H}_2}^0$  (25). From the Arrhenius equation and the Brønsted-Evans-Polanyi



**Fig. 2. Exchange current density of HOR/HER as a function of pH.** (A to D) Exchange current densities ( $i_0$ ) of HOR/HER on (A) Pt/C, (B) Ir/C, (C) Pd/C, and (D) Rh/C as a function of the pH of electrolytes. HOR/HER polarization curves were measured using the RDE method in H<sub>2</sub>-saturated electrolytes at a scanning rate of 1 mV/s and a rotation speed of 1600 rpm at 293 K. Gray stars represent HOR/HER exchange current densities at 293 K estimated from the Arrhenius plot of Durst *et al.* (24), in which all activities were measured using an H<sub>2</sub>-pump configuration.

(BEP) relation, we can derive the following equation (see the Supplementary Materials)

$$i_0 = A \exp\left(-\frac{\beta F E_{\text{peak}}}{RT}\right) \quad (1)$$

where  $A$  is the preexponential coefficient,  $\beta$  characterizes the position of transition state along the reaction coordinate ( $0 < \beta < 1$ ),  $F$  is the Faraday constant (96,485 C/mol),  $R$  is the gas constant [8.314 J/(mol K)], and  $T$  is the temperature in kelvin. This equation is used to fit the  $\log(i_0)$  versus  $E_{\text{peak}}$  data (fig. S7) to obtain  $A$  and  $\beta$  (Table 1). Similar  $\beta$  values (0.5 to 0.8) support the fact that a similar HOR/HER mechanism is at play on all four metals. The preexponential coefficients ( $A$ ) of Pt/C, Ir/C, Pd/C, and Rh/C are also on the same order of magnitude (36 to 59) (Table 1). Note that the  $E_{\text{peak}}$  for Pd/C in Fig. 1 is derived from the second peak because the first peak is not well defined from CVs in most of the electrolytes. Our previous work showed that the sites with weakest HBE were the most active sites for HOR/HER (25); therefore, the lowest  $E_{\text{peak}}$  is the best descriptor to correlate with activity and should be used for the correlation. On the basis of the observation that the peak potential difference between the first and second H<sub>upd</sub> desorption peaks on Pd/C in certain electrolytes is around 0.08 V (fig. S4) and the assumption that the peak potential difference remains roughly

the same in all pH values, as demonstrated in the case of Pt(110) and Pt(100), the potential of the first  $E_{\text{peak}}$  of Pd/C (Fig. 3) is estimated as follows:  $E_{\text{peak, first}} \approx E_{\text{peak, second}} - 0.08$  V.

Activation energies ( $E_a$ ) of HOR/HER on Pt/C, Ir/C, and Pd/C in 0.1 M KOH were determined using the RDE method in this work (fig. S8), and they are greater than those measured in H<sub>2</sub> pumps presumed to be at pH 0 (24) (Table 1). Rh/C does not follow this trend, with similar  $E_a$  observed in 0.1 M KOH and H<sub>2</sub> pumps. Our activation value of  $29.6 \pm 0.4$  kJ/mol on Pt/C in base is in agreement with reported values on polycrystalline Pt ( $28.9 \pm 4.3$  kJ/mol) and Pt/C ( $29.5 \pm 4.0$  kJ/mol) (10). An alternative independent method to obtain  $\beta$  for each metal could be derived from the definition of the BEP relation (eq. S1.2), from which Eq. 2 can be derived (see the Supplementary Materials)

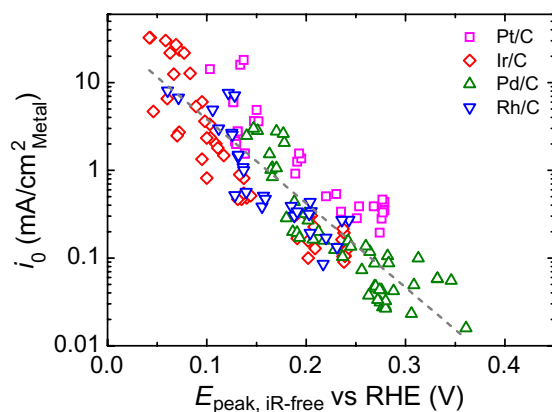
$$\Delta E_a = \beta F \Delta E_{\text{peak}} \quad (2)$$

where  $\Delta E_a$  is the activation energy difference between base and acid [ $E_a$  (0.1 M KOH) -  $E_a$  (H<sub>2</sub> pump)] and  $\Delta E_{\text{peak}}$  is the difference in  $E_{\text{peak}}$  between base and acid [ $E_{\text{peak}}$  (0.1 M KOH) -  $E_{\text{peak}}$  (0.1 M HClO<sub>4</sub>)]. The  $\beta$  values calculated by Eq. 2, denoted  $\beta_{\text{Ea}}$  (Table 1), correspond well with those obtained from  $\log(i_0)$  versus  $E_{\text{peak}}$  fitting, which validates the activity- $E_{\text{peak}}$  correlation. Moreover, this correlation is consistent

with the previous report that Pt(100) has higher HBE and activation energy for HOR/HER than does Pt(110) (26). Hence, it is reasonable to conclude that the higher activation barrier originates from its stronger HBE and is responsible for the slow HOR/HER kinetics in base.

### pH-dependent CO stripping onset potentials

The onset potential of CO stripping on all four metals (Pt/C, Ir/C, Pd/C, and Rh/C) decreases monotonically with pH (Fig. 4), suggesting that coadsorbed OH is unlikely to play a major role in promoting HOR. There is an extensive debate on whether adsorbed OH enhances HOR/HER activity (10–13, 15, 16). The onset potential of CO stripping provides a sensitive measure of the lowest potential at which OH<sub>ad</sub> is present on the surface and, thus, the binding energy of OH<sub>ad</sub>, because OH<sub>ad</sub> facilitates the removal of CO<sub>ad</sub> (16, 27). The onset potential of CO stripping on the four metals decreases with pH (Fig. 4 and figs. S9 to S12), indicating that OH tends to adsorb at a lower potential when the pH is higher. Therefore, if the presence of OH<sub>ad</sub> promotes HOR, higher HOR activity would have been observed at higher pH. However, the opposite trend is observed in Fig. 2. Note that our CO stripping data agree with the results obtained by Gisbert *et al.* (28), with CO stripping on poly-oriented and single-crystal Pt over a wide range of pH (from 2 to 13) in phosphoric acid/phosphate buffer solution. Both the HOR/HER activities and oxophilicity of low-index



**Fig. 3. Correlation between the exchange current density of HOR/HER and H<sub>upd</sub> desorption peak potential.** Exchange current densities of HOR/HER on Pt/C, Ir/C, Pd/C, and Rh/C as a function of the lowest underpotential-deposited hydrogen (H<sub>upd</sub>) desorption peak potential ( $E_{\text{peak}}$ ) from CVs. The gray dashed line represents linear fitting of all data points.

**Table 1. Summary of  $\beta$  and  $A$ .**  $\beta$  and  $A$  from fitting  $i_0$  to  $E_{\text{peak}}$  using the expression  $i_0 = A \exp\left(-\frac{\beta F E_{\text{peak}}}{RT}\right)$ , activation energy ( $E_a$ ) measured using the RDE method in 0.1 M KOH from this work and an H<sub>2</sub>-pump configuration from the study of Durst *et al.* (24), difference in H<sub>upd</sub> desorption peak potentials ( $\Delta E_{\text{peak}}$ ) in 0.1 M KOH and acid with pH 0, and  $\beta_{Ea}$  calculated as  $[E_a(0.1 \text{ M KOH}) - E_a(\text{H}_2 \text{ pump})]/F\Delta E_{\text{peak}}$ .

	$i_0 = A \exp\left(-\frac{\beta F E_{\text{peak}}}{RT}\right)$		$E_a$ (kJ/mol)		$\Delta E_{\text{peak}}$ (V)	$\beta_{Ea}$
	$\beta$	$A$	0.1 M KOH	H <sub>2</sub> pump (pH 0) (24)		
Pt/C	0.5	59	29.6 ± 0.4	16 ± 2	0.17	0.8
Ir/C	0.8	68	32.8 ± 0.4	19 ± 3	0.20	0.7
Pd/C	0.6	37	38.9 ± 3.0	31 ± 2	0.14	0.6
Rh/C	0.6	36	26.6 ± 0.7	28 ± 1	—	—

single-crystal Pt facets have been observed to follow the same sequence of Pt(111) < Pt(100) < Pt(110) (29), which suggests that a more oxophilic surface processes higher activity (29). However, an alternative explanation is that Pt(110) is more active than Pt(100) because it has lower HBE (Fig. 1A). Similarly, the enhanced HOR/HER activity on PtRu as compared to Pt, which has been attributed to the higher oxophilicity of Ru (13), is likely induced by the weakened Pt-H bonding in the presence of neighboring Ru (16). The contradictory trend of HOR/HER activity versus oxophilicity discussed above points to the possibility of no inherent correlation between these two variables.

## DISCUSSION

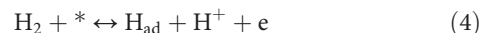
HOR/HER ( $\text{H}_2 \leftrightarrow 2\text{H}^+ + 2\text{e}$  in acid and  $\text{H}_2 + 2\text{OH}^- \leftrightarrow 2\text{H}_2\text{O} + 2\text{e}$  in base) is generally believed to proceed through either a Tafel-Volmer (Eqs. 3, 6, and 7) or a Heyrovsky-Volmer (Eqs. 4 to 7) pathway (30):

### Tafel

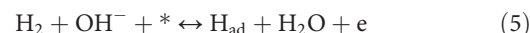


### Heyrovsky

In acid,



In base,

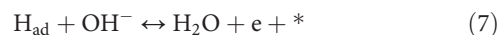


### Volmer

In acid,

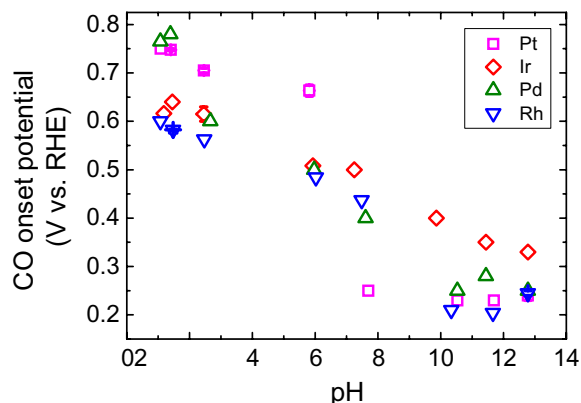


In base,



The universal correlation between  $i_0$  and HBE on the four metals indicates that HOR/HER on those metals may share the same reaction mechanism, that is, the same elementary steps and rate-determining step (RDS). The good fit of the data into the Butler-Volmer equation





**Fig. 4. CO onset potential as a function of pH.** CO stripping onset potentials as a function of pH on Pt/C (magenta squares), Ir/C (red diamonds), Pd/C (olive up triangles), and Rh/C (blue down triangles).

with  $\alpha_a + \alpha_c = 1$  (figs. S2 to S5) suggests that the likely reaction mechanism is the Tafel-Volmer pathway, with the Volmer reaction being the RDS, because a Heyrovsky-Volmer mechanism would have resulted in  $\alpha_a + \alpha_c = 2$  (31). Additional evidence for the Volmer reaction being the RDS includes (i) the excellent correlation between HOR/HER activity and HBE derived from the  $H_{\text{upd}}$  peak potential (11, 15) and (ii) the identical activities determined from HOR/HER measurements and  $H_{\text{upd}}$  charge transfer resistance (11).

A number of theories have been proposed to explain the slower kinetics of HOR/HER in alkaline than in acidic electrolytes. In early studies, Osetrova and Bagotsky (32) suggested that HOR/HER followed a different path in alkaline solutions, that is, through the formation of an  $H_2^+$  intermediate rather than through the dissociative adsorption of  $H_2$ . An alternative theory suggested that the formation of  $H_{\text{ad}}$  is more difficult from  $H_2O$  than from  $H^+$ , which leads to the sluggish kinetics for the reverse reaction of Eq. 7, as compared to that of Eq. 6 (33, 34). However, this hypothesis cannot be applied to HOR because H is abstracted from  $H_2$  instead of  $H^+$  or  $H_2O$ . The potential effects of  $OH_{\text{ad}}$  on HOR in the potential region where  $OH_{\text{ad}}$  is present (above 0.4 V versus RHE based on CO stripping) are (i) site blocking, (ii) modification of HBE through  $H_{\text{upd}}/OH_{\text{ad}}$  interaction (29), and (iii) modification of HBE through  $H_{\text{upd}}/OH^-$  interaction (15). Considering the higher activity in acid than in base (by two orders of magnitude), it is unlikely that the site blocking effect of  $OH_{\text{ad}}$  plays any major role in affecting HOR/HER activity with less than a twofold decrease in ECSA from acid to base. The tuning of HBE is more plausible, as a  $\sim 150$ -mV difference in  $H_{\text{upd}}$  desorption peak potentials has been observed between acid and base electrolytes. Sheng *et al.* (15) proposed that HBE was tuned by  $OH^-$  in the solution phase instead of  $OH_{\text{ad}}$  on the basis of the bare existence of  $OH_{\text{ad}}$  at reversible HOR/HER potential.

Specific adsorption of anions was also found to affect H adsorption; for example, addition of  $Cl^-$  affects the CV of Pt in sulfuric acid by inhibiting the strongly bonded H and shifting the overall curve to cathodic potentials (35). Similarly, Kinoshita *et al.* (36) attributed the stronger H adsorption on Pt in alkaline than in acidic electrolytes to the less extensive specific adsorption of  $OH^-$  than  $HSO_4^-$ . However, this hypothesis cannot explain the difference in the HBE of Pt in  $HClO_4$  and KOH.  $ClO_4^-$  adsorption is weaker than that of  $OH^-$ ; however, the HBE of Pt in  $HClO_4$  is still weaker than that in KOH. Addition

of  $KCl$ ,  $K_2SO_4$ , and  $NaClO_4$  (adsorption strength in the order of  $Cl^- > SO_4^{2-} > ClO_4^-$ ) (29) to 0.1 M KOH while keeping the pH constant leads to only minor changes in the  $E_{\text{peak}}$  (or HBE) (fig. S13, A, C, and E, and table S2) and exchange current densities (fig. S13, B, D, and F), which is consistent with the hypothesis that HBE is the dominant descriptor for HOR/HER activity. The similar dependence of HBE on pH for all four metals indicates that the mechanism through which pH affects HBE is likely to be metal-independent. In this regard, the presence of cations in the immediate vicinity of the electrode surface and their potential interaction with adsorbed H in alkaline electrolytes could be a possible mechanism (29, 37, 38).

Water, the most abundant species in the electrolyte, is ubiquitously adsorbed on the electrode interface (39), which could potentially affect the HOR/HER kinetics or metal-HBE. The presence of water was considered to have little impact on the Pt-H binding energy on the basis of the similar HBE determined electrochemically from temperature-dependent CVs in acid and measured from gas phase in ultrahigh vacuum (UHV) (39–41). However, stronger HBE is obtained in alkaline than in acidic electrolytes, which suggests that the connection between the HBE measured electrochemically and that obtained through UHV techniques may not hold across the whole pH range. Thus, the influence of water may not be excluded. Different orientations of adsorbed water, which is electrode potential- or surface charge-dependent, were mentioned by Trasatti (17), with the oxygen atom in the water molecule pointing toward the metal on a positively charged surface and in an opposite orientation on a negatively charged surface. In electrolytes with different pH values, the electrode surface potential differs in the SHE scale, which might lead to different extents in water dipole orientation or water dipole moments and consequently influence water adsorption/desorption energy. If we consider that the hydrogen adsorption/desorption process in electrolytes is accompanied by displacement/readorption of water molecules, then the apparent HBE might be altered by the adsorption/desorption of water in electrolytes with different pH values. However, further research efforts are needed to evaluate this hypothesis.

The pH dependence of HBE and HOR/HER activities on Pt/C, Ir/C, Pd/C, and Rh/C has been mapped out with cyclic voltammetry and RDE methods in multiple buffer solutions with pH ranging from 0 to 13. Linear correlations between pH and HBE with a similar slope on all four catalysts suggest that the pH dependence of HBE is likely metal-independent.  $\log(i_0)$  decreases linearly with pH and thus HBE, which is consistent with the hypothesis that HBE is the dominant descriptor for HOR/HER catalysts. Low onset potentials of adsorbed OH, characterized by CO stripping experiments, correlate with low HOR/HER activities, indicating that the oxophilicity of metals does not play a significant role in determining HOR/HER activities.

## MATERIALS AND METHODS

### Materials and characterization

Pt/C [5 weight percent (wt %) Pt supported on Vulcan XC-72, Premetek Co.], Ir/C (20 wt % Ir supported on Vulcan XC-72, Premetek Co.), Pd/C (20 wt % Pd supported on Vulcan XC-72, Premetek Co.), and Rh/C (20 wt % Rh supported on Vulcan XC-72, Premetek Co.) were obtained commercially and used as received. Their particle sizes and distributions were examined under a transmission electron microscope (TEM, JEOL 2010F, 200 kV). To prepare TEM samples, Pt/C, Ir/C,

Pd/C, and Rh/C were first added into water and then ultrasonicated for 30 min to form uniform suspensions; a drop of each of the suspensions was then added onto Cu grids (lacy carbon-coated copper grids, Electron Microscopy Sciences) to obtain TEM samples. The diameters of more than 300 Pt, Ir, Pd, and Rh nanoparticles were measured, and their number-averaged sizes and distributions were calculated (fig. S14).

### Preparation of electrolytes

Perchloric acid (HClO<sub>4</sub>; 0.1 and 1 M), sulfuric acid (H<sub>2</sub>SO<sub>4</sub>; 0.1 and 0.2 M), phosphoric acid (H<sub>3</sub>PO<sub>4</sub>; 0.2 M), and acetic acid (CH<sub>3</sub>COOH; 0.2 M) were prepared by diluting 70 wt % HClO<sub>4</sub> (EMD), 95 wt % H<sub>2</sub>SO<sub>4</sub> (EMD), 80 wt % H<sub>3</sub>PO<sub>4</sub> (Sigma-Aldrich), and 99.9% CH<sub>3</sub>COOH (Sigma-Aldrich) with deionized water (18.2 megohms-cm). Potassium hydroxide (KOH; 0.1 and 4 M), citric acid (C<sub>6</sub>H<sub>8</sub>O<sub>7</sub>; 0.2 M), potassium bicarbonate (KHCO<sub>3</sub>; 0.2 M), and boric acid (H<sub>3</sub>BO<sub>3</sub>; 0.2 M) were prepared from KOH tablets (85 wt %, 99.99% metal trace, Sigma-Aldrich), C<sub>6</sub>H<sub>8</sub>O<sub>7</sub> powder (99 wt %, Sigma-Aldrich), KHCO<sub>3</sub> powder (99.7 wt %, Sigma-Aldrich), and H<sub>3</sub>BO<sub>3</sub> powder (99 wt %, Sigma-Aldrich). Buffer solutions were prepared by adding different amounts (1 to 14 ml) of 4 M KOH into 100 ml of 0.2 M solution of C<sub>6</sub>H<sub>8</sub>O<sub>7</sub>, CH<sub>3</sub>COOH, H<sub>3</sub>PO<sub>4</sub>, KHCO<sub>3</sub>, and H<sub>3</sub>BO<sub>3</sub>.

### Electrochemical measurements

Electrochemical measurements were performed in a three-electrode cell with a saturated calomel electrode (SCE; Princeton Applied Research) immersed in a Luggin capillary (Princeton Applied Research) filled with 2 M potassium nitrate (KNO<sub>3</sub>; Sigma-Aldrich) as the reference electrode, a Pt wire (PINE Instrument) as the counter electrode, and a glassy carbon (5-mm diameter, PINE Instrument) as the working electrode. Ink solutions of Pt/C (4 mg<sub>Pt</sub>/ml), Ir/C (1 mg<sub>Ir</sub>/ml), Pd/C (2 mg<sub>Pd</sub>/ml), and Rh/C (1 mg<sub>Rh</sub>/ml) were prepared by dispersing Pt/C, Ir/C, Pd/C, and Rh/C in 0.05 wt % Nafion isopropanol solution followed by ultrasonication for 1 hour. The thin-film electrodes were made by pipetting 2 μl of the ink solutions one, two, or four times onto prepolished glassy carbon electrodes with final metal loadings of 2 to 20 μg<sub>metal</sub>/cm<sup>2</sup><sub>disk</sub>. All reported potentials were converted to an RHE scale.

Cyclic voltammetry measurements for all samples were carried out in Ar-saturated 0.1 M KOH solution, followed by measurements in electrolytes with different pH values at a scanning rate of 50 mV/s. The surface areas of the Pt/C, Ir/C, Pd/C, and Rh/C electrodes were obtained from CVs. The surface areas of Pt, Ir, and Rh were determined from the hydrogen adsorption/desorption peaks with the subtraction of the double layer corresponding to charge densities of 210 μC/cm<sup>2</sup><sub>Pt</sub> (35, 42), 218 μC/cm<sup>2</sup><sub>Ir</sub> (35, 43), and 221 μC/cm<sup>2</sup><sub>Rh</sub> (35, 44), respectively, whereas the surface area of Pd was determined from the PdO reduction peak at about 0.7 V, versus RHE from CVs recorded in the range of 0.07 to 1.25 V, versus RHE corresponding to a charge density of 424 μC/cm<sup>2</sup><sub>Pd</sub> (see the Supplementary Materials and fig. S6) (35, 44).

HOR/HER activity measurements of all samples were performed in H<sub>2</sub>-saturated electrolytes with different pH values at a rotation speed of 1600 rpm. The scanning rate was initially set at 50 mV/s for about five cycles to achieve a stable polarization curve and then changed to 1 mV/s to minimize the influence of capacitance charge. The polarization curves at 1 mV/s were reported and used for calculation of exchange current densities (*i*<sub>0</sub>). The internal resistance (*R*<sub>s</sub>) was measured by electrochemical impedance spectroscopy from 200 kHz

to 100 mHz at open-circuit voltage, which was used to obtain the iR-free potential (*E*<sub>iR-free</sub>) according to the following equation

$$E_{iR-free} = E - IR_s \quad (8)$$

where *E* is the measured potential and *I* is the corresponding current.

The pH values of the electrolytes were calculated from the HOR/HER equilibrium potential (potential at current is equal to zero, *E*<sub>H<sub>2</sub>/H<sup>+</sup> vs. SCE</sub>) as follows, based on the Nernst equation

$$\text{pH} = \frac{-E_{\text{H}_2/\text{H}^+ \text{ vs. SCE}} - E_{\text{SCE}}}{2.303RT/F} \quad (9)$$

where *E*<sub>SCE</sub> is the standard potential for SCE (0.241 V), *R* is the universal gas constant [8.314 J/(mol K)], *T* is the temperature in kelvin, and *F* is the Faraday constant (96,485 C/mol). The reliability of pH determination from the HOR/HER equilibrium potential is verified by its agreement with the corresponding theoretical calculated value (see the Supplementary Materials for detailed calculations and fig. S15).

The HOR/HER activity is represented using exchange current density (*i*<sub>0</sub>), which is obtained by fitting kinetic current (*I*<sub>k</sub>) with the Butler-Volmer equation

$$I_k = i_0 A_s \left[ \exp\left(\frac{\alpha_a F \eta}{RT}\right) - \exp\left(\frac{-\alpha_c F \eta}{RT}\right) \right] \quad (10)$$

where  $\alpha_a$  and  $\alpha_c$  are the transfer coefficients for HOR and HER, respectively, with  $\alpha_a + \alpha_c = 1$ ;  $\eta$  is the overpotential; and *A*<sub>s</sub> is the surface area of the samples.

*I*<sub>k</sub> is calculated using Eqs. 11 and 12 (45)

$$\frac{1}{I} = \frac{1}{I_k} + \frac{1}{I_d} \quad (11)$$

$$\eta_{\text{diffusion}} = -\frac{RT}{2F} \ln\left(1 - \frac{I_d}{I}\right) \quad (12)$$

where *I* is the measured current (in milliamperes); *I*<sub>d</sub> is the diffusion-limited current, defined in Eq. 12; and *I*<sub>l</sub> is the maximum current from polarization curves (in milliamperes).

CO stripping was performed by holding the electrode potential at 0.1 V versus RHE for 10 min in the flowing CO to reach a full monolayer of adsorbed CO on the metal surface and then switching to flow Ar for another 10 min to remove dissolved CO in the electrolyte, followed by cycling in the potential region similar to a normal CV scan at a scan rate of 20 mV/s; the first forward scan represents the stripping of a monolayer of CO. The CO stripping peak can also be used to determine the surface area corresponding to a charge density of 420 μC/cm<sup>2</sup> (46).

### SUPPLEMENTARY MATERIALS

Supplementary material for this article is available at <http://advances.sciencemag.org/cgi/content/full/2/3/e1501602/DC1>

Derivation of relationship between *i*<sub>0</sub> and *E*<sub>peak</sub>

Cyclic voltammograms of Pt/C, Ir/C, Pd/C, and Rh/C at different pH values  
CVs and HOR/HER polarization curves at different pH values

Cyclic voltammograms (CVs)

Correlation of exchange current densities with  $E_{\text{peak}}$

Arrhenius plot

CO stripping in electrolytes with different pH values

Effect of anions on HOR/HER activities

TEM images of supported metal electrocatalysts

Procedure for calculating pH for buffer solutions and comparison between calculated and experimental values

HOR/HER polarization curves on Vulcan XC-72 in electrolytes with different pH values

Fig. S1. CVs of Pt/C, Ir/C, Pd/C, and Rh/C at different pH values.

Fig. S2. CVs and HOR/HER polarization curves at different pH values on Pt/C.

Fig. S3. CVs and HOR/HER polarization curves at different pH values on Ir/C.

Fig. S4. CVs and HOR/HER polarization curves at different pH values on Pd/C.

Fig. S5. CVs and HOR/HER polarization curves at different pH values on Rh/C.

Fig. S6. CVs of Pt/C, Ir/C, Pd/C, and Rh/C in 0.1 M KOH.

Fig. S7. Correlation of exchange current densities with  $E_{\text{peak}}$ .

Fig. S8. Arrhenius plots of HOR/HER activities.

Fig. S9. CO stripping profiles on Pt/C at different pH values.

Fig. S10. CO stripping profiles on Ir/C at different pH values.

Fig. S11. CO stripping profiles on Pd/C at different pH values.

Fig. S12. CO stripping profiles on Rh/C at different pH values.

Fig. S13. Effect of anions on HOR/HER activities.

Fig. S14. TEM images and histograms of Pt, Ir, Pd, and Rh/C.

Fig. S15. Comparison of calculated and electrochemically measured pH of the electrolytes.

Fig. S16. HOR/HER polarization curves on Vulcan XC-72.

Table S1. Particle size and surface area of Pt/C, Ir/C, Pd/C, and Rh/C.

Table S2. Effect of anions on  $H_{\text{upd}}$  peak potentials and HOR/HER exchange current densities.

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